

Fe(III)-catalyzed AGET ATRP of styrene using triphenyl phosphine as ligand

Lifen Zhang · Zhenping Cheng · Zhengbiao Zhang · Deyin Xu · Xiulin Zhu

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Abstract Activators generated by electron transfer for atom transfer radical polymerization (AGET ATRP) is a new technique for conducting ATRP developed recently. In this work, an iron(III)-mediated AGET ATRP of styrene in bulk was carried out at 110 °C, using benzyl bromide as an initiator, oxidatively stable iron(III) chloride hexahydrate ($\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$) as a catalyst, triphenyl phosphine as a ligand, and ascorbic acid as a reducing agent. The polymerizations demonstrated the features of “living”/controlled free-radical polymerization, such as the number-average molecular weights increasing linearly with monomer conversion and narrow molecular weight distributions ($M_w/M_n = 1.14\text{--}1.31$).

Keywords Iron catalyst · AGET ATRP · Styrene · Triphenyl phosphine · Thermal initiation

Introduction

Atom transfer radical polymerization (ATRP), an especially powerful controlled/“living” free-radical polymerization (LRP) technique, has been reported to produce large arrays of polymeric materials with extraordinary control over topologies, composition, microstructures, and functionalities in the last decade [1–6]. However, normal ATRP has some limitation since a relatively unstable lower oxidation state metal catalyst [e.g., Cu(I) or Fe(II)] complex is used, and therefore a special handling procedure to remove the oxygen or other oxidants should be required [7–10]. Recently, the appearance of an improved ATRP, the activators generated by electron transfer (AGET) ATRP [11–22] provides an excellent way to overcome the

L. Zhang · Z. Cheng · Z. Zhang · D. Xu · X. Zhu (✉)
Key Laboratory of Organic Synthesis of Jiangsu Province, College of Chemistry, Chemical Engineering and Materials Science, Soochow (Suzhou) University, 215123 Suzhou, China
e-mail: xlzhu@suda.edu.cn

drawbacks of normal ATRP. In a typical AGET ATRP system, an oxidatively stable Cu(II) complex is used to replace the unstable Cu(I) complex, but the active species Cu(I) complex can be produced by reducing the Cu(II) complex in situ using a reducing agent such as ascorbic acid (VC) or tin(II) 2-ethylhexanoate (Sn(EH)₂) [23–25].

Actually, various metal complexes have been successfully employed to mediate ATRP, including Ti [26], Mo [27, 28], Re [29, 30], Ru [31–34], Rh [35, 36] Ni [37–42], Pd [43], Co [44, 45], Os [46],¹ Cu [47–55], and Fe [56–65]. Complexes of copper have been found to be the most efficient catalysts in the ATRP of a broad range of monomers in diverse media, and the copper-mediated AGET ATRP systems have been intensively reported [11–22]. However, in view of the known toxicity of copper compounds, a more environmentally friendly iron-mediated AGET ATRP system are more appreciated for the synthesis of materials, especially for biomedical applications. As compared with the copper-mediated AGET ATRP, only fewer works involved the iron catalyst. In our previous work, we reported the iron-mediated AGET ATRPs of methyl methacrylate (MMA) using iron(III) chloride hexahydrate (FeCl₃·6H₂O) as the catalyst, iminodiacetic acid [66] or triphenylphosphine (PPh₃) [67] as a ligand and ethyl 2-bromoisobutyrate (EBiB) as an initiator. Luo and Sen [68] also reported an iron-mediated AGET ATRP of styrene and MMA using iron(III) bromide as the catalyst, tributylamine as the ligand, 1-bromoethylbenzene as the initiator, and Sn(EH)₂ or D-glucose as the reducing agent. Very recently, we have reported the iron(III)-mediated AGET ATRP of styrene using a commercially available tris(3,6-dioxahexyl)amine (TDA-1) as the ligand [69, 70] and the iron(III)-mediated surface AGET ATRP of methacrylates [71].

It is well known that, in a ATRP process, ligands play key roles in solubilizing the transition-metal salt in the organic media and in adjusting the redox potential of the metal center for appropriate reactivity and dynamics for the atom transfer [72]. Building on the known use of ligands, nitrogen-based ligands such as 2,2'-bipyridine (bpy) and phosphorus-based ligands are the most frequently used ones. Triphenylphosphine as a simple and cheap ligand was usually used in the iron-mediated normal or reverse ATRP systems. Ibrahim et al. [73] reported a normal ATRP using FeCl₂·4H₂O as the catalyst and PPh₃ as the ligand; and well-defined poly(*n*-butyl methacrylate) (PBMA) homopolymer, or triblock copolymer PMMA-*b*-PEO-*b*-PMMA and PBMA-*b*-PEO-*b*-PBMA [74], were obtained. Hou et al. [75] reported a reverse ATRP of acrylonitrile (AN) using FeCl₃·6H₂O as the catalyst, PPh₃ as the ligand and diethyl 2,3-dicyano-2,3-diphenylsuccinate (DCDPS) as the initiator. However, to the best of our knowledge, there is no any report involved the iron-mediated AGET ATRP of styrene (St) using the phosphorus-based ligand. In this work, the AGET ATRP of St in bulk was investigated using FeCl₃·6H₂O as the catalyst, PPh₃ as the ligand, ascorbic acid as the reducing agent, and benzyl bromide (BB) as the initiator. Well-defined polystyrenes with molecular weights being close to their corresponding theoretical values and narrow molecular weight distributions were obtained by this catalyst system.

Experimental section

Materials

Styrene (>99%), was purchased from Shanghai Chemical Reagents Co. (Shanghai, China). It was washed with an aqueous solution of sodium hydroxide (5 wt%) three times, followed by deionized water until neutralization, and then dried over anhydrous magnesium sulfate, distilled under reduced pressure and stored at $-18\text{ }^{\circ}\text{C}$. $\text{FeCl}_3\cdot 6\text{H}_2\text{O}$ (>99%), PPh_3 (>99%), VC (>99.7%), and BB (analytical reagent) were purchased from Shanghai Chemical Reagents Co. (Shanghai, China) and used as received. Tetrahydrofuran (THF) (analytical reagent) and all other chemicals were obtained from Shanghai Chemical Reagents Co. and used as received unless mentioned.

General procedure for AGET ATRP of St

A typical polymerization procedure for the molar ratio of $[\text{St}]_0/[\text{BB}]_0/[\text{FeCl}_3\cdot 6\text{H}_2\text{O}]_0/[\text{PPh}_3]_0/[\text{VC}]_0 = 200/1/1/3/0.5$ was as follows: $\text{FeCl}_3\cdot 6\text{H}_2\text{O}$ (35.4 mg, 0.131 mmol), PPh_3 (102.9 mg, 0.393 mmol), St (3.0 mL, 26.2 mmol), BB (15.6 μL , 0.131 mmol) and VC (11.6 mg, 0.066 mmol) were added to a dried ampoule under stirring. The ampoule was thoroughly bubbled with argon for 20 min to eliminate the dissolved oxygen in the heterogeneous mixture. The ampoule was flame-sealed and then transferred into an oil bath held by a thermostat at the desired temperature ($110\text{ }^{\circ}\text{C}$) to polymerize under stirring. After the desired polymerization time, the ampoule was cooled by immersing it into iced water. Afterwards, it was opened and the contents were dissolved in THF ($\sim 2\text{ mL}$), precipitated into a large amount of methanol ($\sim 200\text{ mL}$). The polymer obtained by filtration was dried under vacuum until constant weight at $50\text{ }^{\circ}\text{C}$. The monomer conversion was determined gravimetrically. The procedures for other molar ratios of $[\text{St}]_0/[\text{BB}]_0/[\text{FeCl}_3\cdot 6\text{H}_2\text{O}]_0/[\text{PPh}_3]_0/[\text{VC}]_0$ were same as that described above except the different amount of components.

Characterization

The number-average molecular weight ($M_{n,\text{GPC}}$) values and molecular weight distribution (M_w/M_n) values of the polymers were determined using Waters 1515 gel permeation chromatograph (GPC) equipped with a refractive index detector (Waters 2414), using HR 1, HR 2 and HR 4 ($7.8 \times 300\text{ mm}$, $5\text{ }\mu\text{m}$ beads' size) columns with molecular weights ranged $10^2\text{--}5 \times 10^5\text{ g/mol}$. THF was used as an eluent at a flow rate of 1.0 mL/min and $30\text{ }^{\circ}\text{C}$. The GPC samples were injected using a Waters 717 plus autosampler and calibrated with polystyrene standards from Waters. ^1H NMR spectrum was recorded on an Inova 400 MHz nuclear magnetic resonance (NMR) instrument using CDCl_3 as the solvent and tetramethylsilane (TMS) as the internal standard at ambient temperature.

Results and discussion

Polymerization of St at different molar ratios of $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0$

Figure 1 shows the kinetic plot of $\ln([M]_0/[M])$ via time for the AGET ATRP of St in bulk with a molar ratio of $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/0.5$ at 110 °C. A first-order kinetic plot was observed, which indicated that the propagating free-radical concentration was stationary during the polymerization. At the same time, an induction period (4.2 h) was observed in Fig. 1. This phenomenon was also observed in our previous work reported on the iron(III)-mediated AGET ATRP of MMA [67]. Similarly, according to the mechanism of iron(III)-mediated AGET ATRP of MMA, in this work, the active iron(II) complexes were produced by the in situ reduction between the reducing agent VC and the iron(III) complexes, and therefore further produced free-radicals by reversible redox reaction between iron(II) complexes and initiator (BB); subsequently initiate the polymerization of St according to normal ATRP mechanism. In the beginning of polymerization, if not enough Fe(II) complexes were generated duly, the reaction shifted towards left in the presence of a large amount of Fe(III) species, resulting in too low radical concentration to polymerize with the appearance of the induction period [67]. From Fig. 2, the molecular weight ($M_{n,GPC}$) values of the polymers increased linearly with conversion and were close to their corresponding theoretical ones; meanwhile the molecular weight distribution (M_w/M_n) values of the obtained PS remained narrow (less than 1.3).

The reducing agent (i.e., VC) plays an important role in the AGET ATRP process according to the mechanism reported [11, 66, 67]. The effect of VC on the bulk polymerization of St was investigated in this work. The results are listed in Table 1. From the table, it can be seen that even if a low molar ratio of $[Fe(III)]_0/[VC]_0 = 1/0.2$ was used, the polymerization could also be conducted successfully; and that increasing the amount of VC (from a ratio of 1/0.2–1/1.5) the corresponding polymerization rate increased and all the M_w/M_n values kept narrow (~ 1.3), indicating a wide range of the amount of VC can be used. It is noted that the

Fig. 1 $\ln([M]_0/[M])$ and conversion as a function of time for AGET ATRP of St in bulk. Polymerization conditions: $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/0.5$; St = 3 mL; temperature = 110 °C

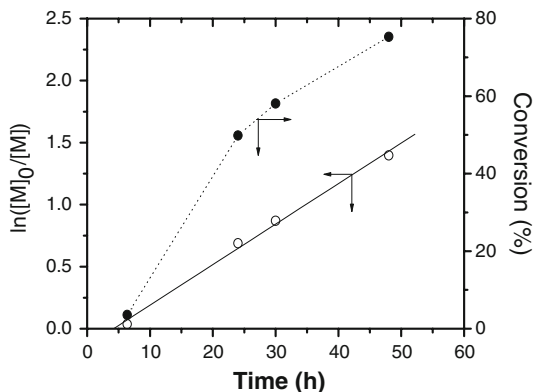
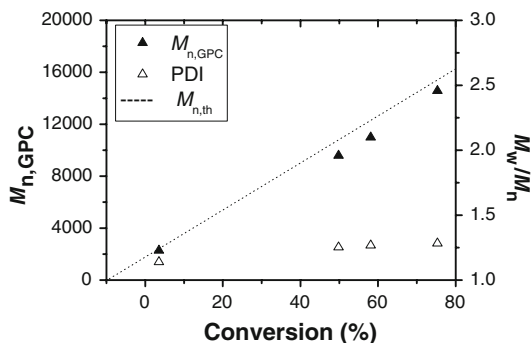


Fig. 2 Average-number molecular weight ($M_{n,GPC}$) and molecular weight distribution (M_w/M_n) versus the conversion for the AGET ATRP of St in bulk. Polymerization conditions: $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/0.5$; $St = 3 \text{ mL}$; temperature = $110 \text{ }^\circ\text{C}$



polymerization of St could also be carried out with a controlled way although no VC was used (Entry 1 in Table 1). However, the polymerization rate in that case is much slower than those in the presence of the reducing agent VC (Entries 2–5 in Table 1). For example, only 13.7% of conversion was obtained for 60 h polymerization time in the absence of the reducing agent VC; while 86.3% of conversion was obtained for 52 h polymerization time in the presence of VC ($[Fe(III)]_0/[VC]_0 = 1/0.5$). Figure 3 shows another polymerization kinetics of AGET ATRP of St in bulk with a molar ratio of $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/1$ at $110 \text{ }^\circ\text{C}$. A first-order kinetic plot like as that with a molar ratio of $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/0.5$ (Fig. 1) indicated the polymerization proceeded with an approximately constant number active species for the duration of the polymerizations up to 89% monomer conversion. In addition, the induction period observed in Fig. 3 shortened to 3.2 h under this polymerization conditions. By calculating the apparent rate constant of polymerization, k_p^{app} ($R_p = -d[M]/dt = k_p[P_n^*][M] = k_p^{app}[M]$), as determined from the kinetic slopes, a k_p^{app} of $9.07 \times 10^{-6} \text{ s}^{-1}$ for the molar ratio of $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/0.5$ (Fig. 1) and another k_p^{app} of $10.4 \times 10^{-6} \text{ s}^{-1}$ for the molar ratio of $[St]_0/[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/1/3/1$ (Fig. 3) were obtained. As expected, increasing the amount of VC increased the polymerization rate (R_p). This is due to that increasing the amount of VC resulted in a higher concentration of Fe(II) salts produced by the in situ reduction of a iron(III) complex with VC. From Fig. 4, the M_w/M_n values of the obtained PSs still kept narrow (1.14–1.31). $M_{n,GPC}$ values increased linearly with conversion, and were close to the corresponding theoretical values, indicating that the iron(III)-mediated AGET ATRP of St was a controlled/“living” radical polymerization.

It is well known that thermal initiation of styrene polymerization usually happens at high temperature (e.g. above $110 \text{ }^\circ\text{C}$) [76–81]. The most widely accepted mechanism for the spontaneous generation of radicals from St was first proposed by Mayo in 1968 [77, 82]. In order to assess the effect of thermal initiation on the AGET ATRP of styrene, reference experiments in the absence of initiator (BB) were carried out. The results are shown in Figs. 5 and 6. A first-order kinetic plot was also observed (Fig. 5); and the molecular weights increased with the monomer conversion while the molecular weight distributions kept narrow (less than 1.30), indicating a controlled polymerization fashion in that case as expected by similarly

Table 1 Effect of the amount of reducing agent on AGET ATRP of St in bulk at 110 °C

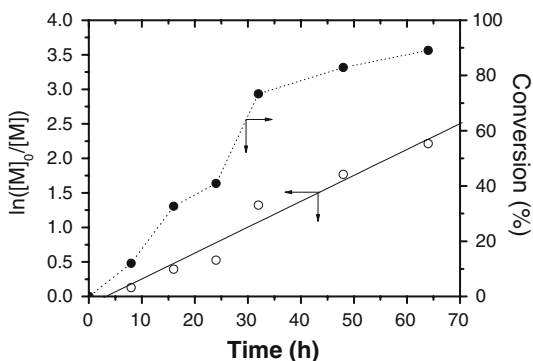
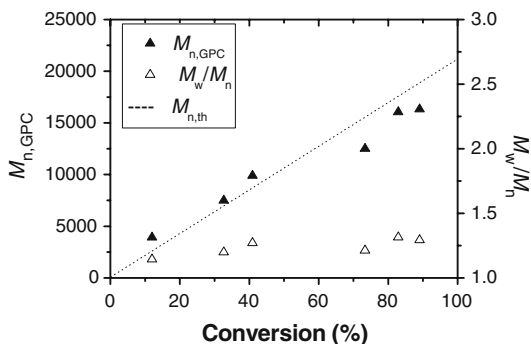
| Entry | R | Time (h) | Conversion (%) | $M_{n,th}^a$ | $M_{n,GPC}$ | M_w/M_n |
|-------|---------------|----------|----------------|--------------|-------------|-----------|
| 1 | 200/1/1/3/0 | 60.0 | 13.7 | 2,850 | 4,280 | 1.30 |
| 2 | 200/1/1/3/0.2 | 66.7 | 81.6 | 16,980 | 13,730 | 1.37 |
| 3 | 200/1/1/3/0.5 | 52 | 86.3 | 17,940 | 13,140 | 1.34 |
| 4 | 200/1/1/3/1.0 | 44.7 | 73.4 | 15,260 | 11,780 | 1.31 |
| 5 | 200/1/1/3/1.5 | 44.2 | 74.0 | 15,400 | 13,020 | 1.29 |

R = [St]₀/[BB]₀/[Fe(III)]₀/[PPh₃]₀/[VC]₀

^a $M_{n,th} = ([St]_0/[BB]_0) \times M_{w,St} \times \text{conversion}\%$

Fig. 3 $\ln([M]_0/[M])$ and conversion as a function of time for AGET ATRP of St in bulk.

Polymerization conditions:
[St]₀/[BB]₀/[FeCl₃·6H₂O]₀/
[PPh₃]₀/[VC]₀ = 200/1/1/3/1;
St = 3 mL;
temperature = 110 °C

**Fig. 4** Average-number molecular weight ($M_{n,GPC}$) and molecular weight distribution (M_w/M_n) versus the conversion for the AGET ATRP of St in bulk. Polymerization conditions: [St]₀/[BB]₀/[FeCl₃·6H₂O]₀/ [PPh₃]₀/[VC]₀ = 200/1/1/3/1; St = 3 mL; temperature = 110 °C

previous work [77]. At the same time, by comparison with the results shown in the Fig. 1, it can be seen that the polymerization rate of the thermal initiation of styrene (in the absence of initiator BB) was slower than that in the presence of initiator BB. For example, a 23.8% of conversion was obtained for the former while a 75.3% of conversion was obtained for the latter after 48 h polymerization time. Thus, thermal initiation of styrene polymerization played a non-negligible role during the AGET ATRP of styrene in that case.

Fig. 5 $\ln([M]_0/[M])$ and conversion as a function of time for AGET ATRP of St in the absence of initiator (BB) in bulk. Polymerization conditions: $[St]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/3/1$; $St = 3 \text{ mL}$; temperature = 110°C

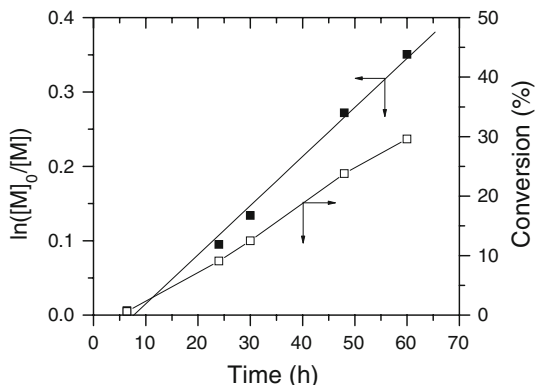
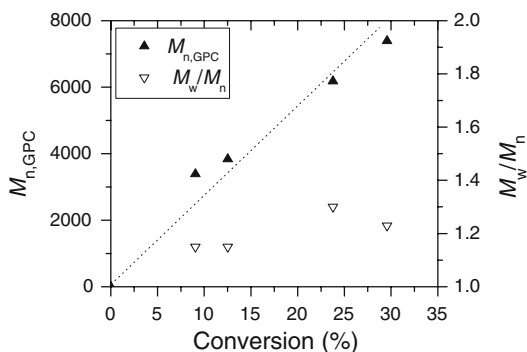


Fig. 6 Average-number molecular weight ($M_{n,GPC}$) and molecular weight distribution (M_w/M_n) versus the conversion for the AGET ATRP of St in the absence of initiator (BB) in bulk. Polymerization conditions: $[St]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0 = 200/1/3/1$; $St = 3 \text{ mL}$; temperature = 110°C



Effect of the amount of $FeCl_3 \cdot 6H_2O$ on polymerization of St

In order to further investigate the effect of Fe(III) concentration on the AGET ATRP of St, 5–100 mol% catalyst relative to the initiator was used. The results are listed in Table 2. From Table 2, it can be seen that when more than 10% catalyst was used, the M_w/M_n values of the obtained PSs kept narrow (less than 1.35); however, when less than 50 mol% catalyst was used, the molecular weights of the obtained PSs deviated from the corresponding theoretical values, which indicated the decrease of controllability over the polymerization of the catalyst system. In addition, when the amount of catalyst was decreased to 5 mol% of the initiator, the M_w/M_n of the obtained PS was 1.6, indicating an uncontrolled polymerization. At the same time, these results showed that the catalyst system was not a very highly active catalyst system. Thus, in order to obtain well-defined PSs, more than 50 mol% catalyst relative to the initiator should be used.

Analysis of chain end

The chain end of the PS was analyzed by 1H NMR spectroscopy, as shown in Fig. 7. The chemical shifts at $\delta = 6.37\text{--}7.08 \text{ ppm}$ (a in Fig. 7) were attributed to the aromatic protons of the BB initiator moieties and PS chains. The chemical shifts at

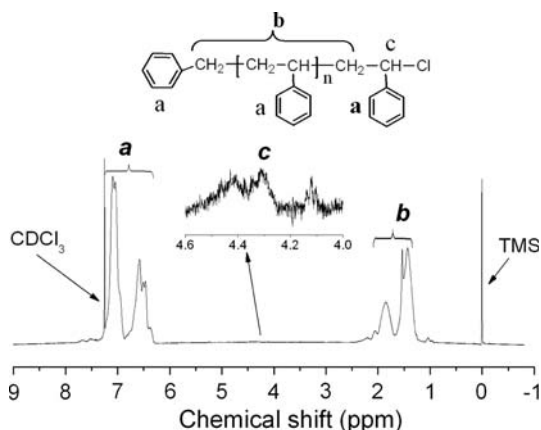
Table 2 Effect of the amount of catalyst on the AGET ATRP of St in bulk at 110 °C

| Entry | R | Time (h) | Conversion (%) | $M_{n,th}^a$ | $M_{n,GPC}$ | M_w/M_n |
|-------|-----------------|----------|----------------|--------------|-------------|-----------|
| 1 | 200/1/1/3/1 | 46 | 76.4 | 15,890 | 14,650 | 1.28 |
| 2 | 200/1/0.5/1.5/1 | 46 | 70.8 | 14,720 | 16,370 | 1.23 |
| 3 | 200/1/0.2/1/1 | 46 | 56.6 | 11,770 | 18,180 | 1.27 |
| 4 | 200/1/0.1/1/1 | 46 | 53.5 | 11,130 | 21,380 | 1.35 |
| 5 | 200/1/0.05/1/1 | 46 | 68.2 | 14,180 | 38,160 | 1.60 |

$$R = [St]_0/[BB]_0/[Fe(III)]_0/[PPh_3]_0/[VC]_0$$

$$^a M_{n,th} = ([St]_0/[BB]_0) \times M_{w,St} \times \text{conversion\%}$$

Fig. 7 1H NMR spectrum of the polymer obtained from AGET ATRP of St in bulk at 110 °C. Sample: $M_{n,GPC} = 12,500$ g/mol, PDI = 1.21



1.42–2.06 ppm (b in Fig. 7) were assigned to the methylene and methyne protons in the PS main chains. The chemical shifts at 4.2–4.5 ppm (c in Fig. 7) were assigned to the methyne protons in the chain ends of PSs because of the electron-attracting function of ω -Cl atom [83], indicating that a ω -Cl atom from catalyst is obtained from $[BB]_0/[FeCl_3 \cdot 6H_2O]_0/[PPh_3]_0/[VC]_0$ initiating system.

Conclusions

A novel method for conducting AGET ATRP of St in bulk mediated by iron(III)/ PPh_3 complexes, using VC as the reducing agent and BB as the initiator, was developed, and it demonstrated the “living”/controlled features. Well-defined polystyrenes with molecular weights being close to their corresponding theoretical values and narrow molecular weight distributions could be obtained when 50–100 mol% catalyst relative to the initiator was used.

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